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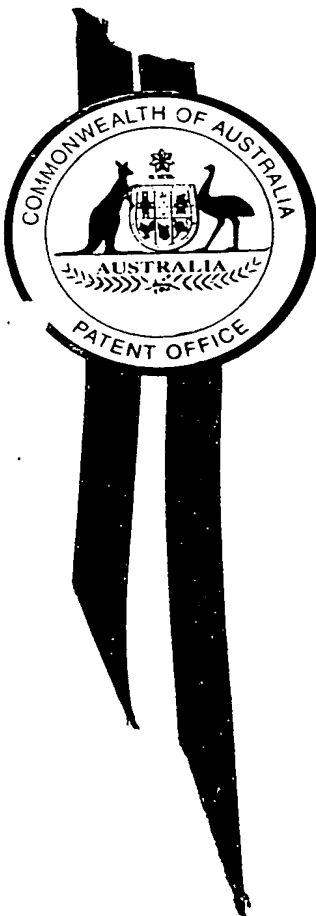
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A U S T R A L I A

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PROVISIONAL SPECIFICATION

for the invention entitled:

"Apparatus and Process"

The invention is described in the following statement:

APPARATUS AND PROCESS

The present invention relates to the baking of carbon, in particular to the baking of carbon
5 anodes such as for use in aluminium smelters. The present invention relates further to a
carbon baking furnace, to a process for the baking of carbon articles and articles so baked.

The conversion of alumina to aluminium metal by electrolysis results in a substantial
consumption of carbon anodes. Molten aluminium is deposited onto a carbon cathode and
10 simultaneously oxygen is deposited on and consumes the carbon anode of the electrolytic cell.
Typically, up to 0.4 tonnes of carbon are consumed for every tonne of aluminium produced.
As a result, aluminium smelters have a requirement for a substantial and continuous supply
of carbon electrode. Most smelters manufacture carbon anodes as an integral part of the
aluminium production process.

15

The manufacture of carbon anodes comprises producing "green" anode blocks and baking the
"green" blocks to produce anodes suitable for use. The production of "green" blocks involves
the mixing of crushed coke or anthracite and a binding agent which, for example, contains
coal tar pitch. The viscous mixture is then pressed to form "green" anode blocks. Depending
20 on the smelters' requirements, "green" anodes may weigh between a few hundred kilograms
to more than a tonne. The mixture of coke and pitch binder is solid at room temperature and
softens at temperatures over about 50°C. Volatile components are released at temperatures
between 50°C and 400°C. When subjected to further heating over a period of time, to about
1200°C, the anode hardens, resulting in improved physical properties, such as electrical
25 conductivity and resistance to oxidation.

Carbon baking furnaces are often referred to as ring-type furnaces where "green" anode
blocks are loaded into large pits, covered with sacrificial coke and baked. The furnace is
generally a concrete tub lined with refractory materials to provide a number of pits into which
30 a column of green anodes may be loaded for baking, usually about six deep. Each pit is

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typically surrounded by two flues for heating the anodes, the flue-walls also being lined with refractory materials. As each pit is loaded, "green" anodes are packed in with sacrificial coke. These furnaces typically require baking cycles of about 2 to 3 weeks which includes preheating and the time that the baked anode is left in the pit to cool prior to removal.

5

The thermal cycling of these types of carbon baking furnaces causes adverse effects on the refractory materials, concrete and other ceramic components. The refractory materials change with heat and time, resulting in altered brick dimensions. Further packing coke material may lodge into expansion gaps. This, together with temperature cycling, leads to large structural deformation of walls and ultimately failure.

Deformed flue walls must be regularly replaced as excessive tub-wall deformation results in an inefficient operation and necessitates furnace rebuilding. Costs associated with regular flue-wall replacement and maintenance of joints and tub-walls can be as high as 50% of the overall anode baking costs.

According to the present invention there is now provided a carbon baking furnace comprising a refractory lined kiln defining the baking path, further comprising a means for substantially continuously receiving green carbon articles, means for packing said green carbon articles in a sacrificial medium, a means for the substantially continuous displacement of the packed carbon articles through said baking path and a means for substantially continuously removing baked carbon articles from the kiln.

In a second aspect there is provided a process for baking carbon articles, said process comprising the steps of substantially continuously loading green carbon articles into a refractory lined kiln, said kiln defining a baking path, packing said green carbon articles in a sacrificial medium, substantially continuously displacing the carbon articles through said baking path and substantially continuously removing baked carbon articles from the kiln.

Advantageously, the present invention provides carbon articles which have been subjected to

more consistent temperature treatments. This results in articles of improved baked quality. In the manufacture of baked carbon anodes for use in aluminium smelting operations, improved baked quality contributes significantly to cell efficiency. Temperature gradients in excess of 150°C in a single pit of ring type furnaces are not uncommon. Such high
5 temperature gradients may result in thermo-mechanical degradation of the anode matrix. The present invention may reduce or eliminate cracking due to high temperature gradients in the baking process.

Furthermore, the present invention allows all structural materials such as refractories,
10 concrete supports and other ceramic products to be maintained at relatively constant temperatures, substantially reducing thermal cycling of these materials. The furnace may then be able to operate for longer periods without requiring extensive maintenance. Furnace rebuilds costing tens of millions of dollars are standard in ring-type furnaces. Such rebuilds may take place at approximately five- yearly intervals. As thermal cycling of refractories will
15 be substantially reduced according to the present invention, the useful life of the furnace will be greatly extended.

It will be understood that the term "substantially continuously" refers to a continuous mode of operation whereby carbon articles are passed continuously through the kiln. The rate at
20 which the carbon articles are passed through the kiln may be uniform or may involve a periodic or step-wise passage through the kiln. This will be determined primarily by the means for receiving and removing the articles from the kiln.

The refractory lined kiln may be any convenient refractory lined kiln which is capable of
25 heating the carbon articles up to temperatures of about 1200°C to 1300°C. Preferably the refractory lined kiln may comprise a number of heating zones whereby each heating zone is capable of maintaining the carbon articles to a desired temperature for a desired period. Refractories may be selected according to the heating zone in the kiln in which they are intended for use. For example, in the preheat/volatiles extraction zone low permeability
30 refractories with high resistance to volatiles attack, such as those refractories used in

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incinerators are preferred. In high temperature zone refractories with high resistance to thermomechanical degradation are preferred. Alumina silicates (greater than 45% alumina) are also useful in the other zones of the kiln.

5 The refractories may include guides such as protrusions, to position the carbon articles within the baking path defined by the refractory lined kiln. It is desirable that the baking path be substantially straight so as to permit the carbon articles to be conveyed along the baking path with a minimum requirement for actuators or conveyors to operate or be located within the kiln.

10

Preferably the kiln defines a vertical baking path whereby the carbon articles are displaced downwardly through the baking path as a result of the weight of the carbon articles and the weight of the sacrificial medium and other carbon articles. The rate at which the carbon articles pass through the baking path may conveniently be regulated by substantially
15 continuously removing the bottom most baked carbon article from the kiln in a manner whereby the weight of the carbon articles and the sacrificial medium is supported within the kiln and the remaining carbon articles are substantially continuously displaced through the baking path.

20 Alternatively the kiln may define a substantially horizontal baking path or a baking path on an inclined plane whereby the carbon articles are substantially continuously displaced through the baking path by a push rod or other convenient means.

Preferably the kiln may comprise a number of heating zones in order to facilitate the control
25 of temperature in the carbon articles. Improved control of temperature permits when more even heat treatment of the carbon articles and the manufacture of carbon articles having higher baked quality. It is preferable that the kiln comprise a first heating zone whereby the carbon article is heated to a temperature whereby any volatile materials are volatilised.

30 Conveniently, means for extracting any volatile materials may be incorporated into this first

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heating zone and extracted from the kiln. The extraction of volatile organic compounds from the kiln permits these potentially toxic compounds to be contained and optionally pumped, with the fuel, into the heating zones of the kiln. This minimises the likelihood of any emissions of volatile materials such as pitch fumes from the furnace into the environment.

5 Furthermore the containment of pitch fumes is particularly desirable as pitch condensates are extremely difficult to handle and costly to eliminate.

Second and subsequent heating zones may control the rate of increase of the temperature of the carbon articles as they substantially continuously pass through the baking path. The rate

10 at which the carbon articles pass through the baking path and the configuration of the heating zones in the kiln will determine the heat treatment profile to which the carbon articles are subjected.

The means for substantially continuously receiving green carbon articles may be any

15 convenient means, dependent on the configuration and orientation of the refractory lined kiln and the baking path. We have found that the use of a conveyor and a hydraulic ram is particularly suited to a kiln having a vertical baking path wherein the green carbon articles are received at the top of the kiln. The conveyor may position the green carbon article adjacent to the top of the kiln and the hydraulic ram place the green carbon article into the

20 baking path.

The means for packing the green carbon articles in a sacrificial medium may be any convenient means dependent on the morphology of the sacrificial medium. Preferably the sacrificial medium is a friable packing coke. The means for packing the green carbon articles

25 in a friable sacrificial medium may include a hopper fitted with a suitable nozzle whereby the sacrificial medium is spread over and around the green carbon article. Preferably the sacrificial medium occupies the remaining space in the kiln once the carbon articles have been located therein. It is desirable to reduce the amount of free space in the kiln.

30 Refractory spacers are preferably used to separate the carbon articles in the kiln so as to

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prevent the carbon articles being baked together and to alleviate difficulties in separating the baked carbon articles. Suitable spacers may be made from consumable materials such as aluminium sheets, cardboard, or paper. Alternatively the spacers may be made from refractory or carbonaceous materials. These spacers may be reused or recycled.

5

The means for the substantially continuous displacement of the carbon articles through the baking path may include means whereby the carbon articles are forced or pushed through the baking path. Preferably, gravity is used to urge the carbon articles through the baking path and the substantially continued displacement of the carbon articles is achieved by retarding
10 or braking the movement of the lower or lowest carbon articles thereby exercising control over the rate at which the carbon articles pass down the kiln.

The means for substantially continuously removing the baked carbon article from the kiln may be any convenient means depending on the configuration and orientation of the kiln. In the
15 preferred configuration and orientation of the kiln where the baking path is substantially vertical and the carbon articles pass down the kiln under their own weight and the weight of the sacrificial medium, a preferred means for substantially continuously removing the baked carbon articles from the kiln includes the use of hydraulic rams and conveyor belts. The bottom-most baked carbon article is preferably supported by one hydraulic ram while the
20 adjacent baked carbon article is engaged by a second pair of opposed rams so as to restrain or support all but the bottom-most baked carbon article. The bottom-most baked carbon article is then lowered by the first mentioned hydraulic ram onto a conveyor belt for storage and/or use.

25 The sacrificial medium may be any medium which will protect the carbon articles. The sacrificial medium may preferentially react with or absorb the oxygen in the kiln prior to its reaction with the carbon in the articles being baked. It is preferred that the sacrificial medium be friable to permit it easy incorporation around the carbon articles and to permit the easy movement of the carbon articles within the kiln. The sacrificial medium may be selected so
30 as to provide an optimum balance of rendering the carbon articles easily moveable through

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the furnace and providing sufficient protection of the carbon articles from oxygen contained within the kiln. Preferably the sacrificial medium is packing coke having a particle size having a maximum particle size of less than 15mm.

- 5 It is also desirable for the sacrificial medium to conduct heat efficiently to the carbon articles. For this reason, it is desirable that the amount of sacrificial medium used is sufficient to provide adequate protection for the carbon articles from oxygen, permit the easy movement of the carbon articles in the kiln and to provide efficient heat transfer.
- 10 Desirably the sacrificial medium may be collected from the furnace and, so far as is capable, be recycled for packing further green carbon articles. For example, the flow of this medium may be controlled by the use of a pendulous carbon trough, the flow rate being proportional to the period of oscillation.
- 15 The furnaces of the present invention may be arranged such that a plurality of such furnaces are positioned adjacent to one another so as to permit the efficient use of equipment and heating values in the fuel.

Throughout this specification and the claims which follow, unless the context requires
20 otherwise, the word "comprise", or variations such as "comprises" or "comprising", will be understood to imply the inclusion of a stated integer or group of integers but not the exclusion of any other integer or group of integers.

The present invention will now be further described with reference to the accompanying
25 drawings. In the drawings the carbon articles are represented by anodes for use in the aluminium smelting industry. It will be understood that the present invention applies equally to the baking of other carbon articles.

Figure 1 is a cross sectional view of the carbon baking furnace of the present invention.

30 Figure 2 is a cutaway perspective diagram of a preferred embodiment of the carbon baking

furnace of the present invention.

The carbon baking furnace(1) shown in Figure 1 incorporates a refractory lined kiln(2) and a heating means(4). Green carbon anodes(3) are encased in packing coke(6) and are substantially continuously fed through the heating zone generated by the heating means(4). Baked carbon anodes(5) are produced after passing through the heating zone. Means for receiving green carbon anodes (not shown) and means for removing baked carbon anodes (not shown) assist to control the rate at which the anodes pass through the heating zone and the temperature profile to which they are subjected.

10

Figure 2 shows a preferred configuration of the carbon baking furnace of the present invention. Figure 2 is a cutaway perspective drawing. Green carbon anodes(3) are positioned adjacent the refractory lined kiln(2) by conveyor belt(7). Hydraulic rams(8) position the green carbon anodes (3) over the baking path of refractory lined kiln(2). The bottom-most baked carbon anode(5) is lowered by hydraulic ram(9) after the adjacent carbon anode(10) is engaged by hydraulic rams(11). Baked carbon anode (5) is then positioned by hydraulic ram(9) on conveyor belt(12) for storage and/or use. Hydraulic ram(9) engages baked carbon anode(10), hydraulic rams (11) disengage baked carbon anode(10) and hydraulic ram(9) lowers baked carbon anode(10) into the position previously occupied by baked carbon anode(5) as a result the column of anodes moves downwards in a substantially continuous manner.

Green carbon anode(3) is positioned on a spacing element(13). Packing coke(6) is then fed by hopper(14) through nozzle(15) to fill the space surrounding the green carbon anode(3) in the kiln(2). As the carbon anodes pass through the kiln(2) the carbon anodes enter a volatile extraction zone(16). Volatiles such as pitch fumes are extracted through holes in the refractory materials(17) through extraction unit(18). The extracted fumes are fed into the heating unit(19) in addition to fuel in order to provide sufficient calorific values to raise the temperature of the carbon anodes to the desired baking temperature. The fuel is fed into the heating unit(19) through nozzle(20).

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After the anodes have passed through the high temperature zone adjacent to the heating unit(19) the packing coke(6) is removed from the baked anodes by scrapers(21). The packing coke(6) which has been removed from the baked carbon anodes is then transported on conveyor belts(23) and (24) and returned to the hoppers(14) via continuous buckets(25) and 5 conveyor belt(26).

Advantageously the substantially continuous flow of anodes and coke through the carbon baking furnace eliminates the need for expensive and labour intensive loading and unloading procedures as in existing furnace designs. Large multipurpose cranes costing more than 10% 10 of the overall capital budget of ring type furnaces requiring high ongoing operating costs may be eliminated. The present invention permits a fully automated anode and packing coke loading and unloading system, along with the resultant increased productivity.

Defined thermal gradients along the carbon baking furnace make it possible to separate 15 heating and volatile extraction zones. This facilitates fuel efficiency and the responsible handling of toxic organic volatiles. The baking column may be operated at an equilibrium temperature with little or no thermal cycling. Fuel otherwise spent in the reheating of furnace components in ring-type furnaces may be eliminated. In the carbon baking furnace of the present invention fuel will only be used to provide the necessary calorific values required to 20 bake the anodes (not heating and reheating refractory substructures).

Volatiles may be extracted and pumped into the heating zone the carbon baking furnace for the complete combustion of toxic organic compounds. Current technologies, due to design limitations are unable to fully combust or efficiently contain these toxins. Pitch fumes escape 25 from the furnace environment or condense within the ringmains. Pitch condensates are extremely difficult to handle and are costly to eliminate. The present invention makes it possible to reduce the risk of exposing workers to highly toxic substances.

Current carbon baking furnace designs operate within narrow parameters, the distance 30 between the anodes and flue walls is critical to achieving optimum baking. In the past this

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inflexibility has presented operators with costly refurbishment when anode design changes are required. The carbon baking furnace of the present invention may more easily be modified to control carbon anode temperature, such as by varying the rate at which they are passed through the various temperature zones and the temperature of said zones furthermore, baking
5 temperatures may be optimised to improve in anode baking.

The carbon baking furnace of the present invention is able to accommodate anodes of varying size with minimal structural change. Temperature profiles can be tailored by altering configuration of the columns heat exchange systems.

10

A stacked, one anode deep column is preferred as it provides a thermally efficient design. In general, the continuous furnace of the present invention will require approximately one fifth of the surface area needed to accommodate an equivalent ring-type furnace. The continuous furnace of the present invention may typically be between 20m and 30m high,
15 with anode velocities between 3 and 4.5m/day.

Advantageously, the carbon baking furnace of the present invention may result in a significant reduction in fuel consumption, more uniform baking of anodes and efficient toxic volatiles elimination.

20

We have found that anode deformation, otherwise known as "slumping", during baking is insignificant. Green anodes subjected to loads at varying temperatures reveal dimensional instability in the 25°C to 150°C temperature range. This is directly related to the temperature zone at which anode volatiles are emitted. Test results show that all samples (regardless of
25 load) maintain their structural integrity at temperatures beyond 150°C and the degree of permanent deformation is less than 0.5%

Those skilled in the art will appreciate that the invention described herein is susceptible to variations and modifications other than those specifically described. It is to be understood
30 that the invention includes all such variations and modifications which fall within its spirit and

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scope. The invention also includes all of the steps, features, compositions and compounds referred to or indicated in this specification, individually or collectively, and any and all combinations of any two or more of said steps or features.

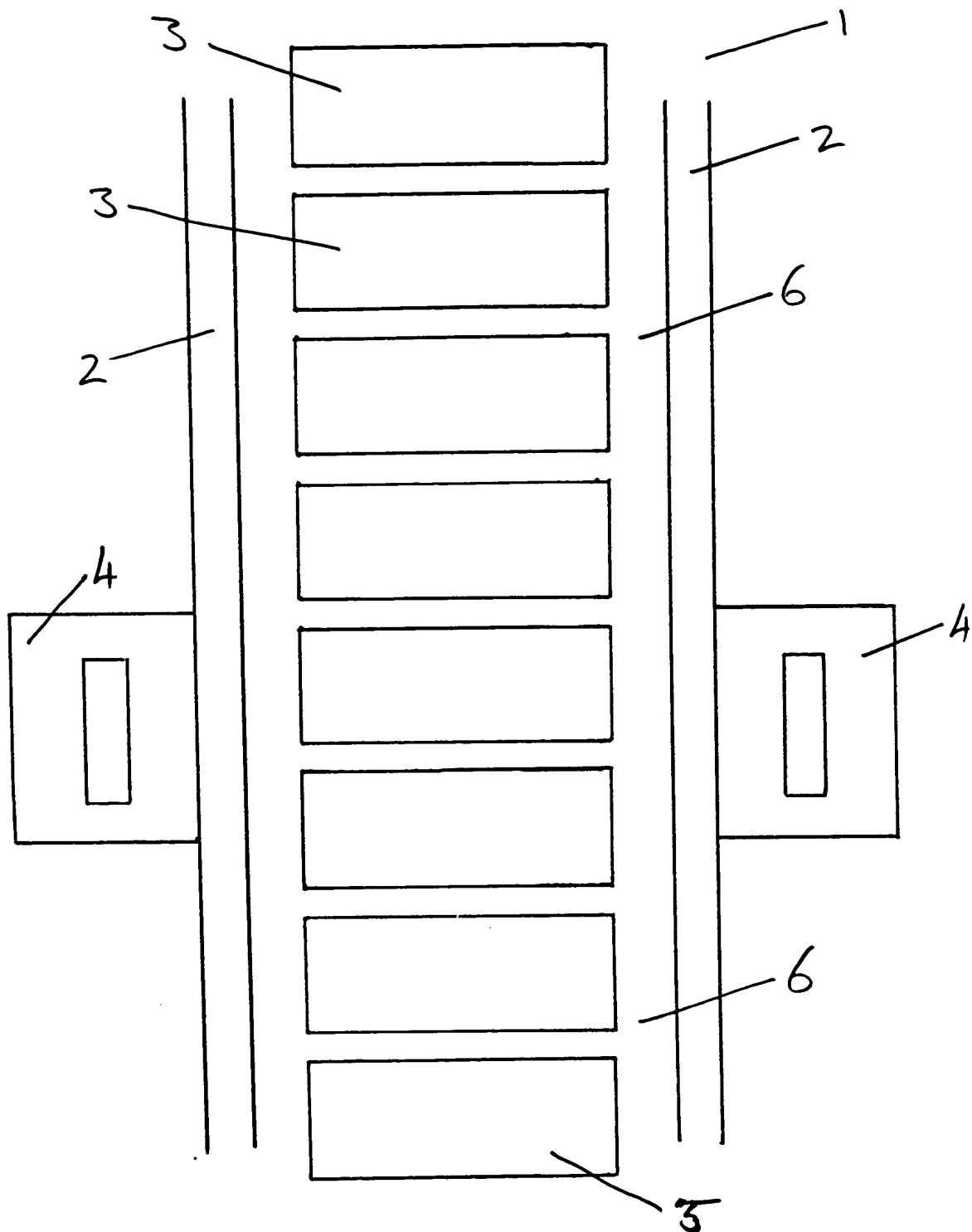
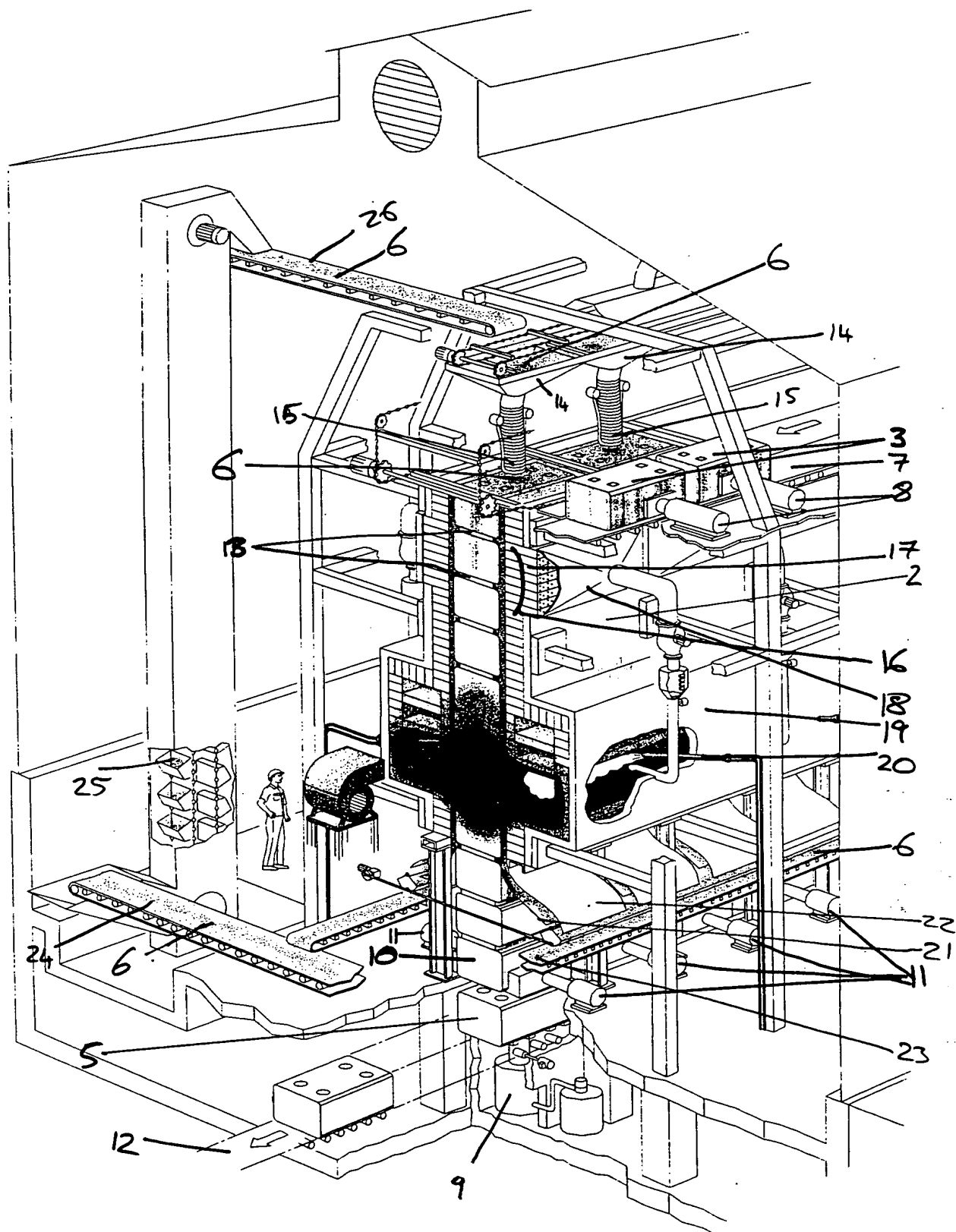


FIG 1



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